

2015 DPD Workshop

September 21-23, 2015, Shanghai University

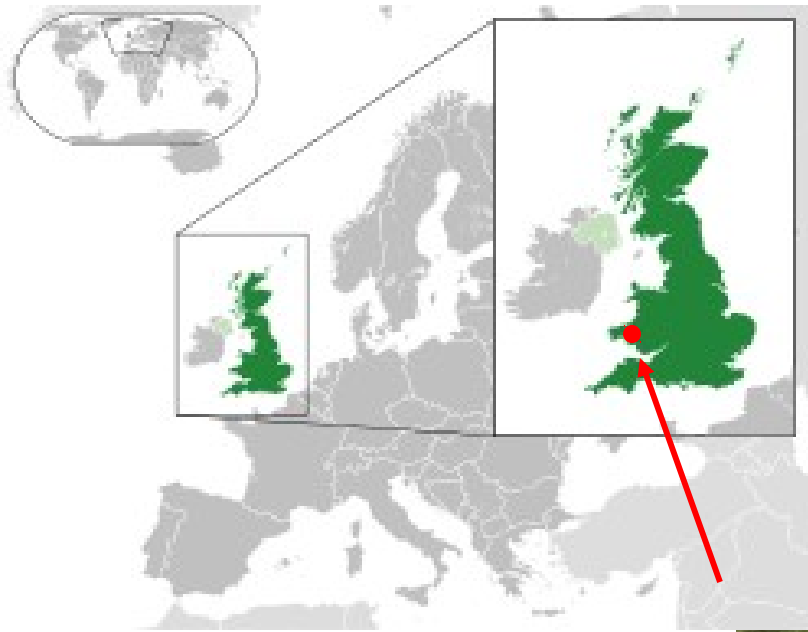
Smoothed Dissipative Particle Dynamics: *theory and applications to complex fluids*

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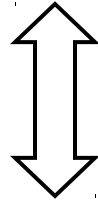


Acknowledgments

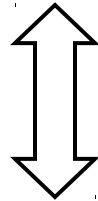
- * Pep Español (UNED Madrid)
- * Nikolaus Adams (TUM)
- * Adolfo Vazquez-Quesada (Swansea U.)
- * Xiangyu Hu (TUM)
- * Xin Bian (Brown U.)
- * Sergey Litvinov (ETH)

Outline:

Smoothed Particle Hydrodynamics (continuum)



Smoothed Dissipative Particle Dynamics



Dissipative Particle Dynamics (mesoscopic)

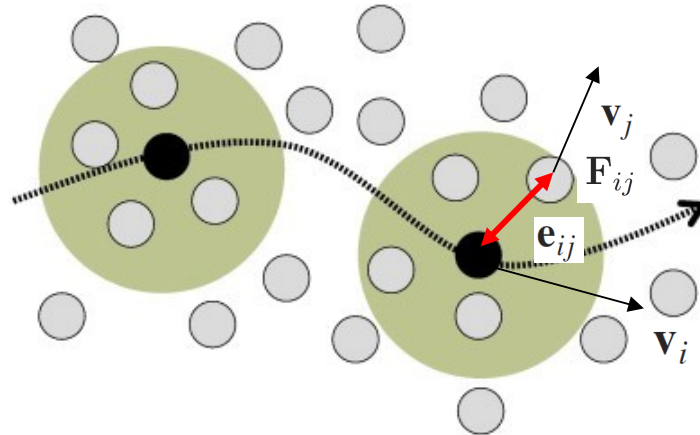
Part I: theory

I. What is S-DPD?

Smoothed Dissipative Particle Dynamics

Smoothed Dissipative Particle Dynamics (**SDPD**)
 Español, Revenga, Phys. Rev E, *E* **67**: 026705 (2003)

$$\begin{aligned} \dot{\mathbf{r}}_i &= \mathbf{v}_i \\ m\dot{\mathbf{v}}_i &= - \underbrace{\sum_j \left(\frac{P_i}{d_i^2} + \frac{P_j}{d_j^2} \right) W'_{ij} \mathbf{e}_{ij}}_{\mathbf{F}_{ij}^C} + \underbrace{\frac{5\eta}{3} \sum_j \frac{W'_{ij}}{d_i d_j r_{ij}} [\mathbf{v}_{ij} + (\mathbf{e}_{ij} \cdot \mathbf{v}_{ij}) \mathbf{e}_{ij}]}_{\mathbf{F}_{ij}^D} + \sum_j \underbrace{A_{ij} \frac{d\bar{\boldsymbol{\xi}}_{ij}}{dt} \cdot \mathbf{e}_{ij}}_{\mathbf{F}_{ij}^R} \end{aligned}$$



Smoothed Dissipative Particle Dynamics

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General Equation for Non-Equilibrium Reversible-Irreversible Coupling (**GENERIC**)
Öttinger, Grmela Phys. Rev E, *E* **56**: 6620–6632 (1997)

$$d\mathbf{x} = \mathbf{L} \cdot \frac{\partial E}{\partial \mathbf{x}} dt$$

□ Total energy E conserved (1st Law Thermodynamics)

Smoothed Dissipative Particle Dynamics

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$$d\mathbf{x} = \mathbf{L} \cdot \frac{\partial E}{\partial \mathbf{x}} dt + \mathbf{M} \cdot \frac{\partial S}{\partial \mathbf{x}} dt$$

- ❑ **Total energy E conserved (1st Law Thermodynamics)**
- ❑ **Monotonic entropy increase S (2nd Law Thermodynamics)**

Smoothed Dissipative Particle Dynamics

Smoothed Dissipative Particle Dynamics (**SDPD**)
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General Equation for Non-Equilibrium Reversible-Irreversible Coupling (**GENERIC**)
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$$d\mathbf{x} = \mathbf{L} \cdot \frac{\partial E}{\partial \mathbf{x}} dt + \mathbf{M} \cdot \frac{\partial S}{\partial \mathbf{x}} dt + d\tilde{\mathbf{x}}$$

- ❑ **Total energy E conserved (1st Law Thermodynamics)**
- ❑ **Monotonic entropy increase S (2nd Law Thermodynamics)**
- ❑ **Fluctuation Dissipation Theorem (FDT)**

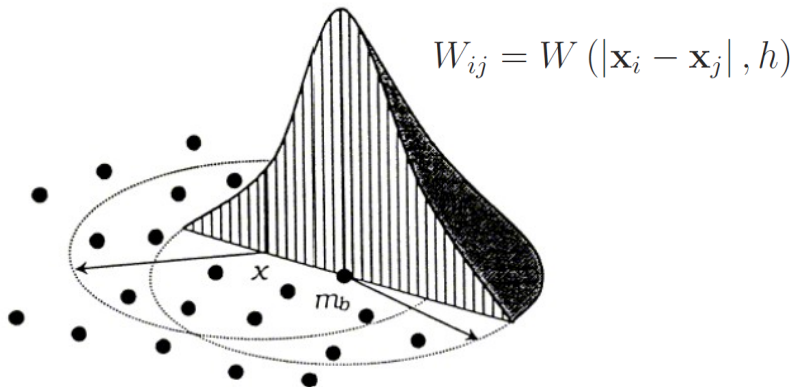
$$d\tilde{\mathbf{x}} d\tilde{\mathbf{x}}^T = 2k_B \mathbf{M} dt$$

Conservative (pressure) forces

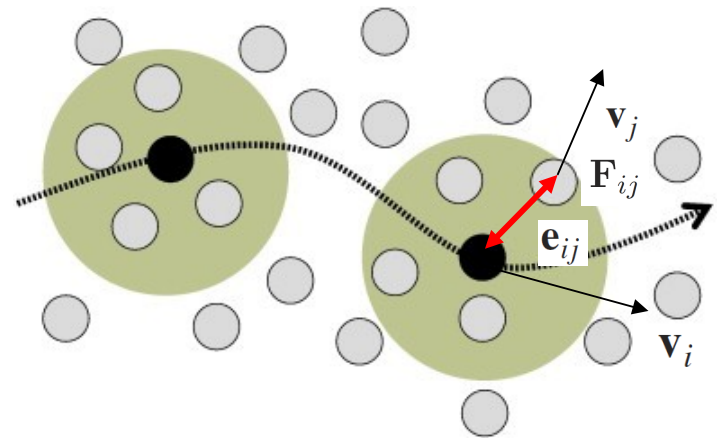
$$\underbrace{\left(\frac{P_i}{d_i^2} + \frac{P_j}{d_j^2} \right) W'_{ij} \mathbf{e}_{ij}}_{\mathbf{F}_{ij}^C}$$

Fluid particle density/volume

$$d_i = \frac{1}{\mathcal{V}_i} = \frac{\rho_i}{m_i} = \sum_j W_{ij} \longrightarrow P(\rho)$$



Non-local repulsive forces



Conservative (pressure) forces

$$\left(\frac{P_i}{d_i^2} + \frac{P_j}{d_j^2} \right) W'_{ij} \mathbf{e}_{ij}$$

Discrete representation **pressure gradient** (Euler equations):
Smoothed Particle Hydrodynamics

$$f_i = \sum_j \mathcal{V}_j f_j W_{ij} \longrightarrow \nabla f_i = \sum_j \mathcal{V}_j f_j \underbrace{\nabla_i W_{ij}}_{W'_{ij} \mathbf{e}_{ij}}$$

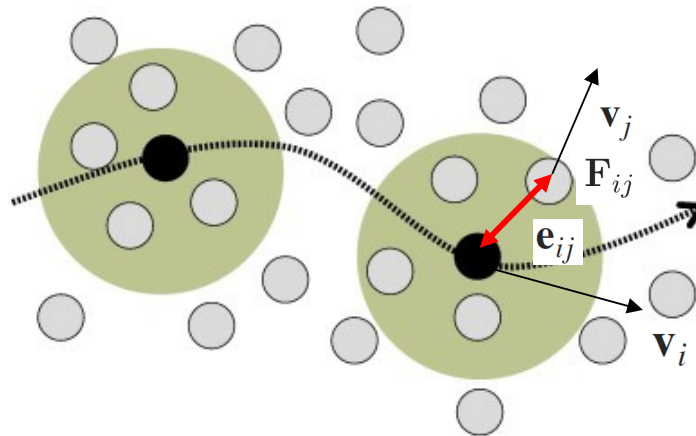
$$\frac{\nabla p}{\rho} = \nabla \left(\frac{p}{\rho} \right) - \frac{p}{\rho^2} \nabla \rho$$

L.B. Lucy, *Astron. J.* 82 (12) (1977) 1013–1924.

R.A. Gingold, J.J. Monaghan, *Monthly Notices Roy. Astron. Soc.* 181 (1977) 375–389.

Dissipative (viscous) forces

$$\underbrace{\frac{W'_{ij}}{d_i d_j r_{ij}} [\mathbf{v}_{ij} + (\mathbf{e}_{ij} \cdot \mathbf{v}_{ij}) \mathbf{e}_{ij}]}_{\mathbf{F}_{ij}^D}$$



Dissipative (viscous) forces

$$\frac{5\eta}{3} \sum_j \frac{W'_{ij}}{d_i d_j r_{ij}} [\mathbf{v}_{ij} + (\mathbf{e}_{ij} \cdot \mathbf{v}_{ij}) \mathbf{e}_{ij}]$$

Discrete representation **viscous dissipation** (Navier-Stokes equations):
Smoothed Particle Hydrodynamics

Random forces

$$\underbrace{A_{ij} \frac{d\bar{\xi}_{ij}}{dt} \cdot \mathbf{e}_{ij}}_{\mathbf{F}_{ij}^R}$$

Matrix independent Wiener process

$$d\bar{\xi}_{ij} = \frac{1}{2} (d\xi_{ij} + d\xi_{ij}^T)$$

$$\langle d\xi_{ij}^{\alpha\beta} \rangle = 0$$

$$\langle \xi_{ij}^{\alpha\alpha'} \xi_{i'j'}^{\beta\beta'}(t') \rangle = (\delta_{ii'} \delta_{jj'} + \delta_{ij'} \delta_{ji'}) \delta^{\alpha\beta} \delta^{\alpha'\beta'} dt$$

SDPD – Fluctuation Dissipation Theorem

$$d\tilde{\mathbf{x}} d\tilde{\mathbf{x}}^T = 2k_B \mathbf{M} dt$$

$$A_{ij} = \left[-\frac{20}{3} k_B T \eta \frac{W'_{ij}}{d_i d_j r_{ij}} \right]^{1/2}$$

Smoothed Dissipative Particle Dynamics

Similar to **Dissipative Particle Dynamics**

$$\begin{aligned}\dot{\mathbf{r}}_i &= \mathbf{v}_i \\ m\dot{\mathbf{v}}_i &= - \sum_j \underbrace{\left(\frac{P_i}{d_i^2} + \frac{P_j}{d_j^2} \right) W'_{ij} \mathbf{e}_{ij}}_{\mathbf{F}_{ij}^C} + \frac{5\eta}{3} \sum_j \underbrace{\frac{W'_{ij}}{d_i d_j r_{ij}} [\mathbf{v}_{ij} + (\mathbf{e}_{ij} \cdot \mathbf{v}_{ij}) \mathbf{e}_{ij}]}_{\mathbf{F}_{ij}^D} + \sum_j \underbrace{A_{ij} \frac{d\bar{\boldsymbol{\xi}}_{ij}}{dt} \cdot \mathbf{e}_{ij}}_{\mathbf{F}_{ij}^R}\end{aligned}$$

.. but connected to **Smoothed Particle Hydrodynamics**

$$\begin{aligned}\dot{\mathbf{r}}_i &= \mathbf{v}_i \\ m\dot{\mathbf{v}}_i &= - \underbrace{\sum_j \left(\frac{P_i}{d_i^2} + \frac{P_j}{d_j^2} \right) W'_{ij} \mathbf{e}_{ij}}_{(\nabla p / \rho)_i} + \underbrace{\frac{5\eta}{3} \sum_j \frac{W'_{ij}}{d_i d_j r_{ij}} [\mathbf{v}_{ij} + (\mathbf{e}_{ij} \cdot \mathbf{v}_{ij}) \mathbf{e}_{ij}]}_{\eta \nabla^2 \mathbf{v}_i + (\eta/3) \nabla(\nabla \cdot \mathbf{v}_i)}\end{aligned}$$

II. SDPD: meso or macro method?

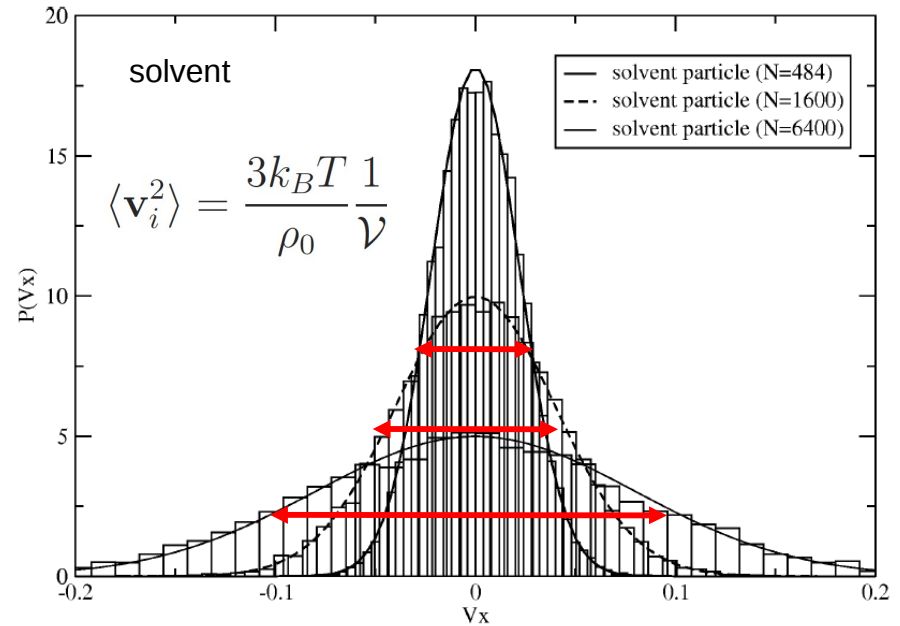
Consistent scaling SDPD thermal fluctuations

Vazquez, Ellero, Español, J. Chem. Phys. **130**: 034901 (2009)

Maxwell-Boltzmann velocity distribution
variance

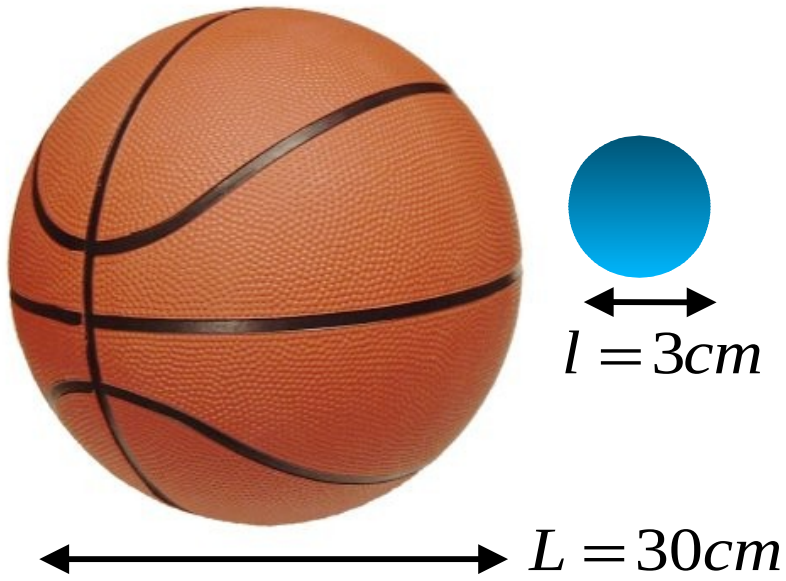
$$\langle \mathbf{v}_i^2 \rangle = \frac{3k_B T}{\rho_0 \mathcal{V}}$$

$$\mathcal{V}_i = \left(\sum_j W_{ij} \right)^{-1}$$

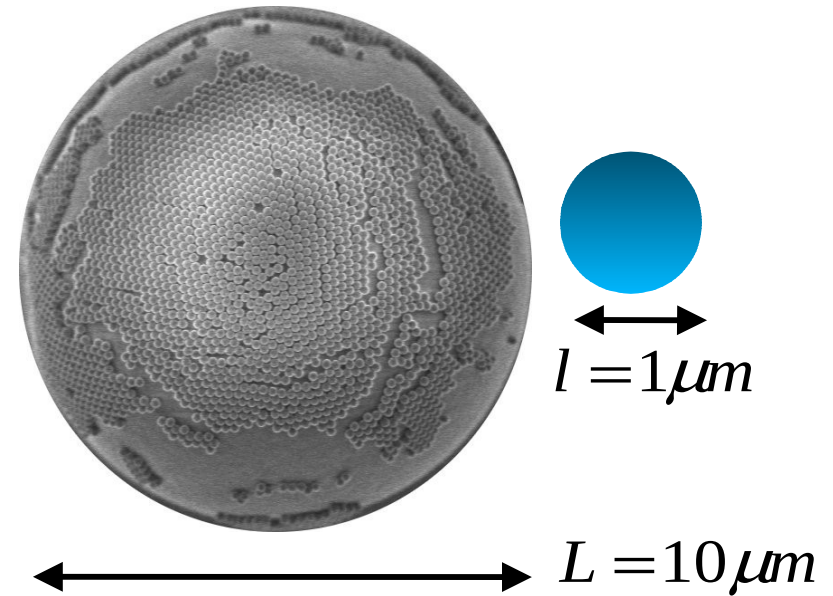


Consistent scaling SDPD thermal fluctuations

Vazquez, Ellero, Español, J. Chem. Phys. **130**: 034901 (2009)



$$\langle v_i^2 \rangle = D \frac{k_B T}{\rho_0} \frac{1}{V} \approx 0$$



$$\langle v_i^2 \rangle = D \frac{k_B T}{\rho_0} \frac{1}{V} \neq 0$$

Consistent scaling SDPD thermal fluctuations

Vazquez, Ellero, Español, J. Chem. Phys. **130**: 034901 (2009)

$$\begin{aligned}\dot{\mathbf{r}}_i &= \mathbf{v}_i \\ m\dot{\mathbf{v}}_i &= -\sum_j \left(\frac{P_i}{d_i^2} + \frac{P_j}{d_j^2} \right) W'_{ij} \mathbf{e}_{ij} + \frac{5\eta}{3} \sum_j \frac{W'_{ij}}{d_i d_j r_{ij}} [\mathbf{v}_{ij} + (\mathbf{e}_{ij} \cdot \mathbf{v}_{ij}) \mathbf{e}_{ij}] + \sum_j A_{ij} \underbrace{\frac{d\bar{\boldsymbol{\xi}}_{ij}}{dt}}_{\mathbf{F}_{ij}^R} \cdot \mathbf{e}_{ij}\end{aligned}$$

$$\mathcal{V}_i = \left(\sum_j W_{ij} \right)^{-1} \longrightarrow \infty \qquad \longrightarrow 0$$

Fluid particle volume

$$\lim_{\mathcal{V}_i \rightarrow \infty} \text{SDPD} = \text{SPH}$$

IV. Advantages in using S-DPD?

Solvent properties specification

DPD

Thermodynamic behaviour
(Equation of State)

$$P(\rho) = \rho k_B T + \alpha a \rho^2$$

Groot, Warren, J. Chem. Phys. **107**, 4423 (1997)

- $\nu = \frac{45k_B T}{4\pi\gamma\rho r_c^3} + \frac{2\pi\gamma\rho r_c^5}{1575}$
- $c_s = \sqrt{k_B T + 2\alpha a \rho}$

Groot, Warren, J. Chem. Phys. **107**, 4423 (1997)

Transport coefficients

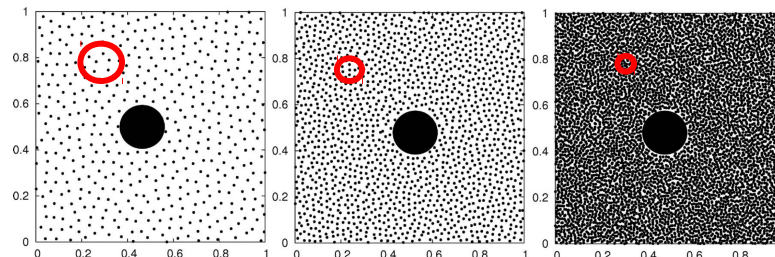
SDPD

- $P(\rho) = c_s^2 \rho$
- $P(\rho) = P_o \left[\left(\frac{\rho}{\rho_0} \right)^\gamma + B \right]$
- $P(\rho) = \frac{\rho k_B T}{1 - A\rho} - B\rho^2$

- $\nu = \frac{\eta}{\rho_0}$
- c_s

Scaling particle volumes, resolution analysis

Difficult to preserve physical quantities :Ma, Re, Sc,
(depend on particle size)



Specified once for all.

Independent fluid particle size

V. SDPD accuracy?

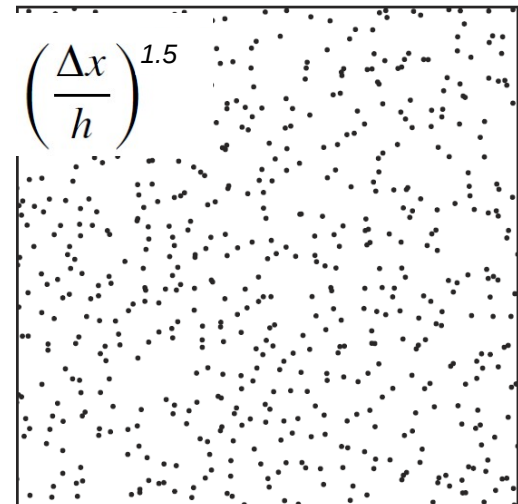
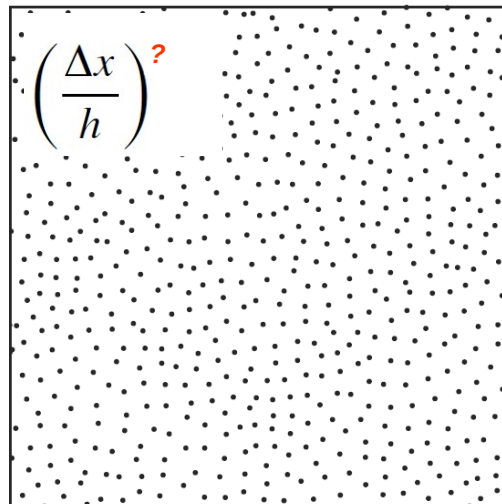
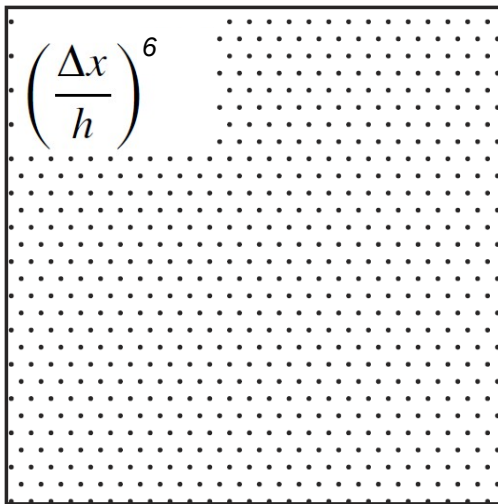
Approximation/convergence SDPD-SPH

$$f(\mathbf{r}) \longrightarrow \underbrace{\langle f(\mathbf{r}) \rangle_h = \int f(\mathbf{r}') W(|\mathbf{r} - \mathbf{r}'|) d\mathbf{r}'}_{\text{Mollification: smoothing kernel}} \longrightarrow \underbrace{\langle f(\mathbf{r}) \rangle_h^\Delta = \sum_{j=1}^N \nu_j f(\mathbf{r}_j) W(|\mathbf{r} - \mathbf{r}_j|)}_{\text{Quadrature}}$$

Errors

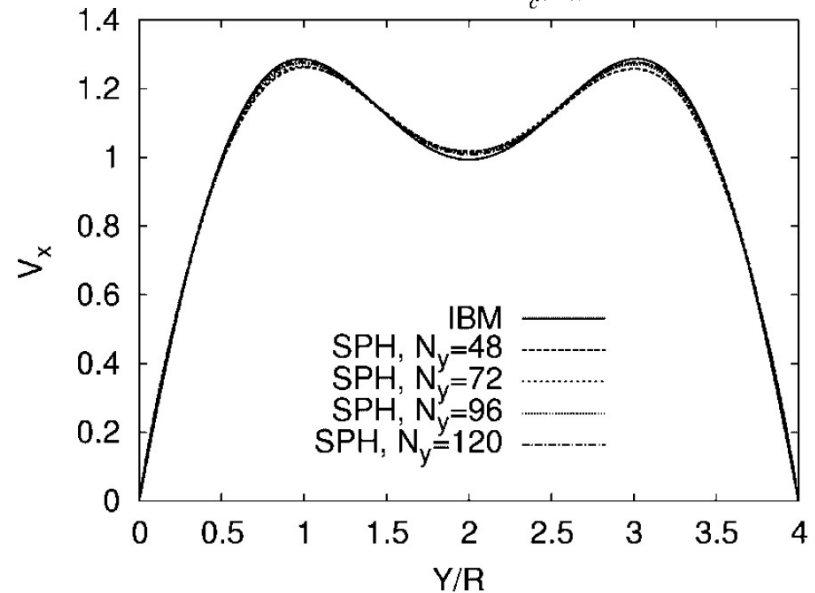
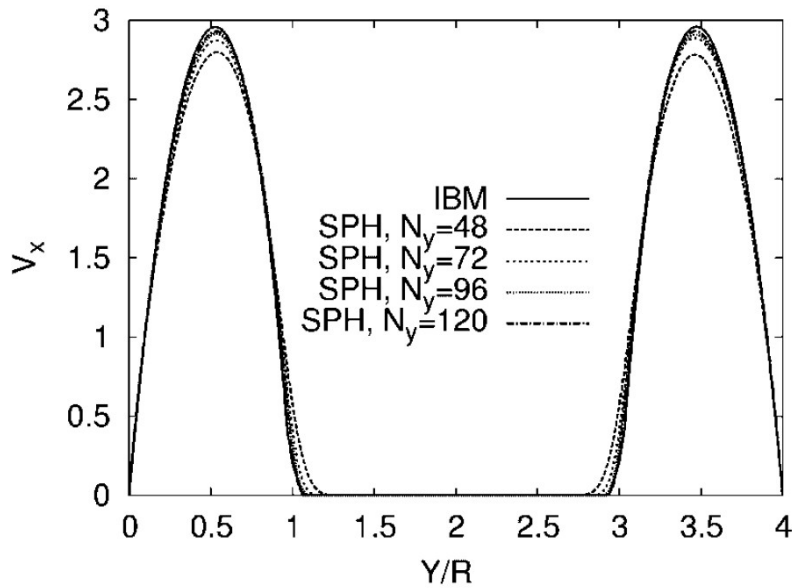
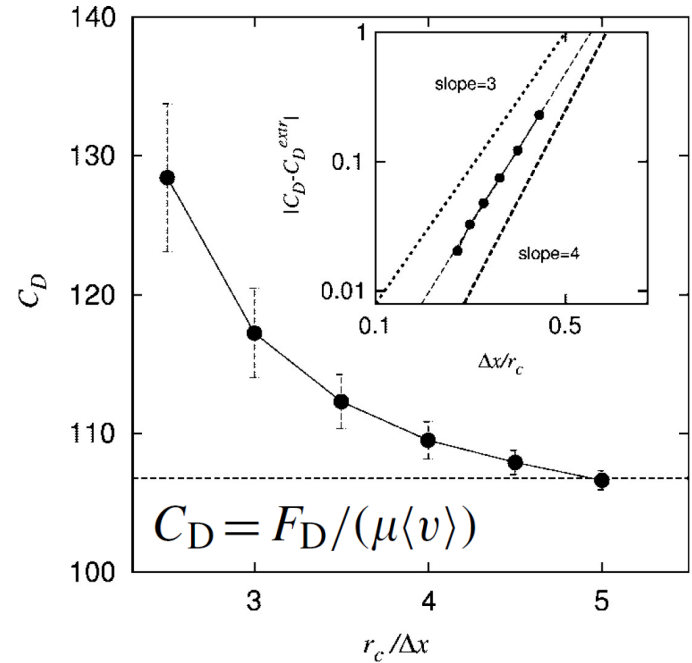
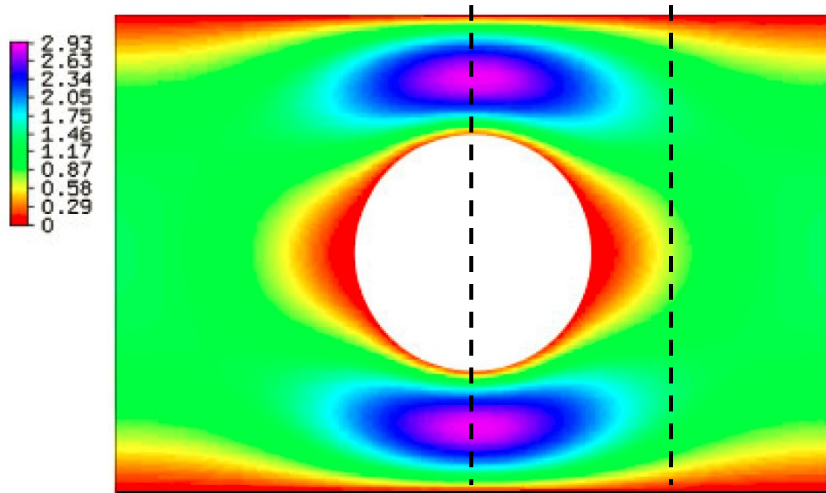
$$\|f(\mathbf{r}) - \langle f(\mathbf{r}) \rangle_h^\Delta\| = \mathcal{O}\left(\left(\frac{h}{L}\right)^n\right) + \mathcal{O}\left(\left(\frac{\Delta}{h}\right)^m\right)$$

- $n = 2$ radially-symmetric kernel
- $m = \begin{cases} 3/2, & \text{random} \\ \approx 3, & \text{structured} \\ \beta + 4, & \text{lattice} \end{cases}$



Approximation/convergence SDPD-SPH

Ellero, Adams, Int. J. Num. Meth. Engng. **86**, 1027 (2011)



VI. SDPD slower than DPD ?

SDPD vs DPD: algorithmic complexity

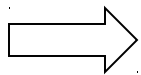
$$\begin{aligned}\dot{\mathbf{r}}_i &= \mathbf{v}_i \\ m\dot{\mathbf{v}}_i &= \sum_j \mathbf{F}_{ij}^C + \sum_j \mathbf{F}_{ij}^D + \sum_j \mathbf{F}_{ij}^R\end{aligned}$$

DPD

$$\begin{aligned}\mathbf{F}_{ij}^C &= a_{ij} \max(1 - r_{ij}/r_c, 0) \\ \mathbf{F}_{ij}^D &= \gamma \omega^D(r_{ij}) (\mathbf{e}_{ij} \cdot \mathbf{v}_{ij}) \mathbf{e}_{ij} \\ \mathbf{F}_{ij}^R &= \sigma \omega^R(r_{ij}) \xi_{ij} \mathbf{e}_{ij}\end{aligned}$$

SDPD

$$\begin{aligned}\mathbf{F}_{ij}^C &= \left(\frac{P_i}{d_i^2} + \frac{P_j}{d_j^2} \right) W'_{ij} \mathbf{e}_{ij} \\ \mathbf{F}_{ij}^D &= \frac{W'_{ij}}{d_i d_j r_{ij}} [\mathbf{v}_{ij} + (\mathbf{e}_{ij} \cdot \mathbf{v}_{ij}) \mathbf{e}_{ij}] \\ \mathbf{F}_{ij}^R &= A_{ij} \frac{d\bar{\xi}_{ij}}{dt} \cdot \mathbf{e}_{ij}\end{aligned}$$



$$\begin{aligned}\square \quad d_i &= \frac{1}{\mathcal{V}_i} = \sum_i W_{ij} && \text{extra density evaluation} \\ \square \quad d\bar{\xi}_{ij} &= \frac{1}{2} (d\xi_{ij} + d\xi_{ij}^T) && \text{tensorial Wiener process}\end{aligned}$$

SDPD vs DPD: algorithmic complexity

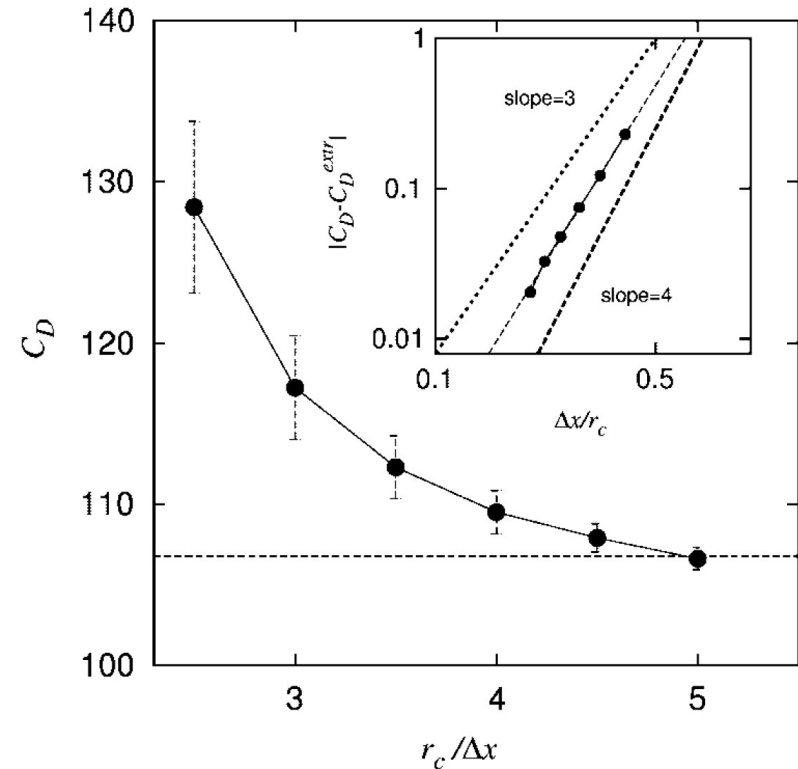
- Number of neighbours/particle (2D)

$$\frac{h}{\Delta} = 2 \longrightarrow N_{neigh} \approx 12$$

$$\frac{h}{\Delta} = 3 \longrightarrow N_{neigh} \approx 27$$

$$\frac{h}{\Delta} = 4 \longrightarrow N_{neigh} \approx 48$$

Ellero, Adams, Int. J. Num. Meth. Engng. **86**, 1027 (2011)



- Large # neighbours required only for exact specification transport coefficients
- If less accuracy is required, one can run with same # neighbors as DPD.

Part II: complex fluids

SDPD: hierarchical modelling of complex fluids



□ **I: Mesoscopic**

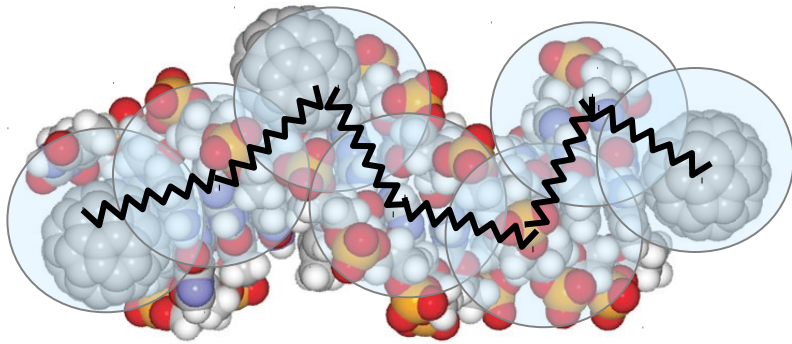
□ **II. Coarse-graining**

□ **III. Macroscopic**

I: Mesoscopic

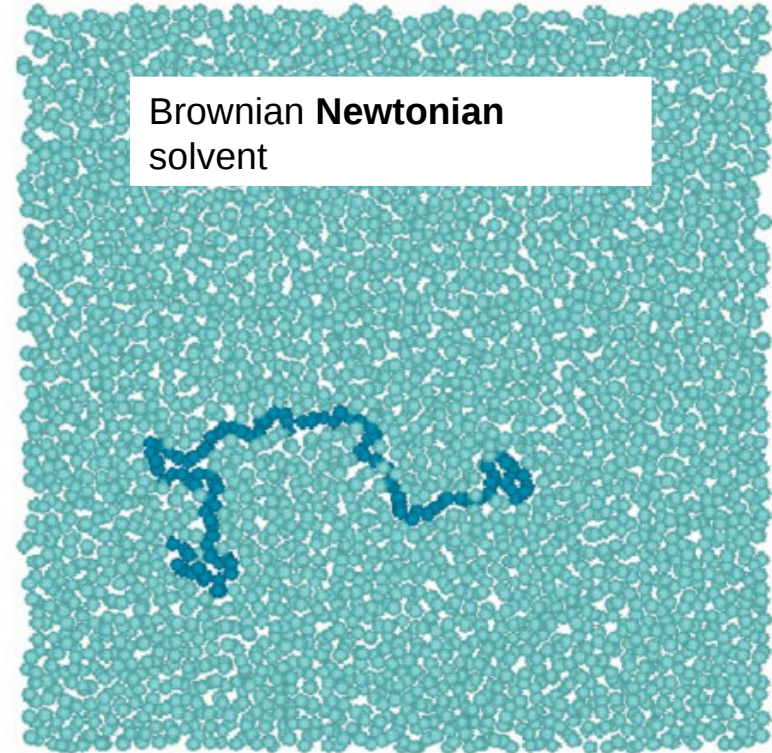
Polymeric fluid: *mesoscopic* model

Litvinov et al., Phys.Rev. E 77, 66703 (2008)



$$m_i \frac{d\mathbf{v}_i}{dt} = \mathbf{F}_i^{\text{hydro}} + \mathbf{F}_{i,i_1}^{\text{FENE}} + \mathbf{F}_{i,i_2}^{\text{FENE}}$$

$$\mathbf{F}^{\text{FENE}}(\mathbf{r}_{ij}) = \frac{K\mathbf{r}_{ij}}{1 - (r/R_0)^2}$$

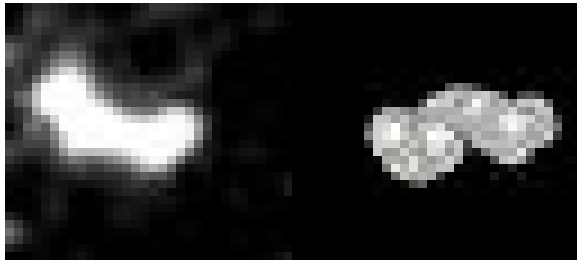


- excluded volume effect: self-avoidance
- correct hydrodynamics interactions
- preserved chain topology
- finite extensibility

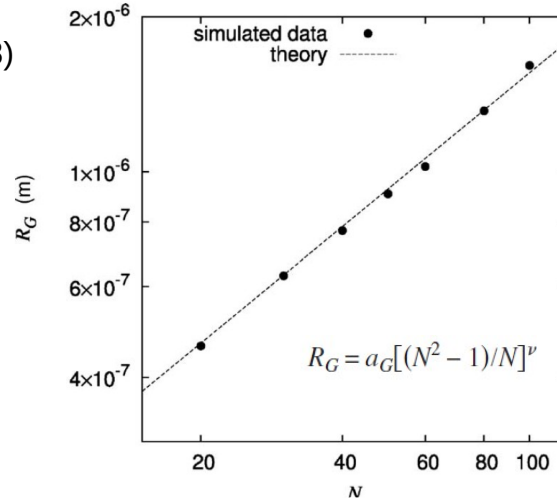
Polymeric fluid: *mesoscopic* model

Equilibrium properties

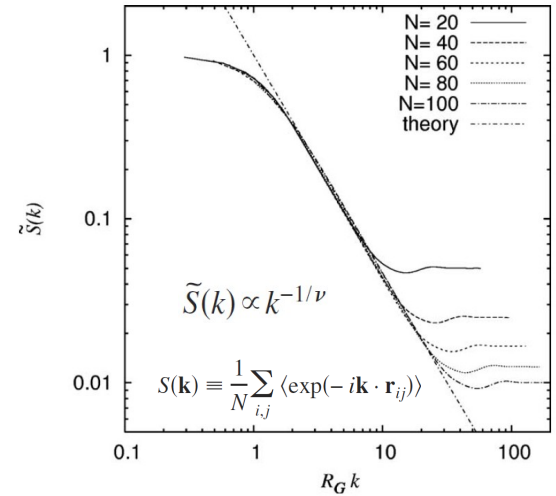
Litvinov et al., Phys.Rev. E **77**, 66703 (2008)



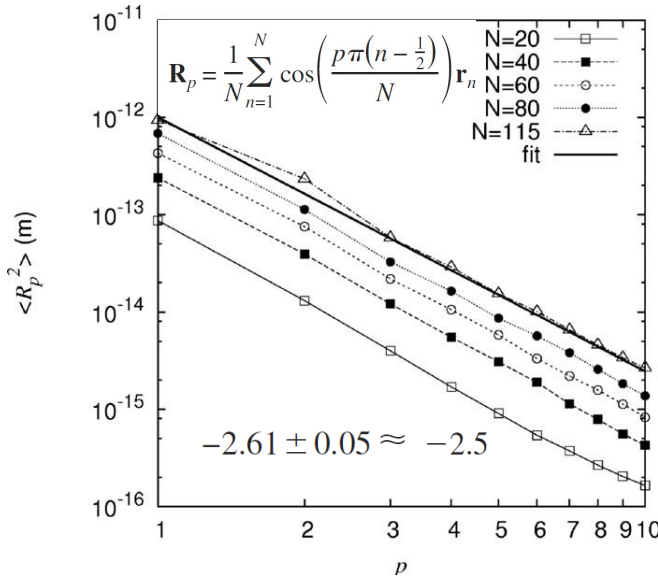
gyration radius



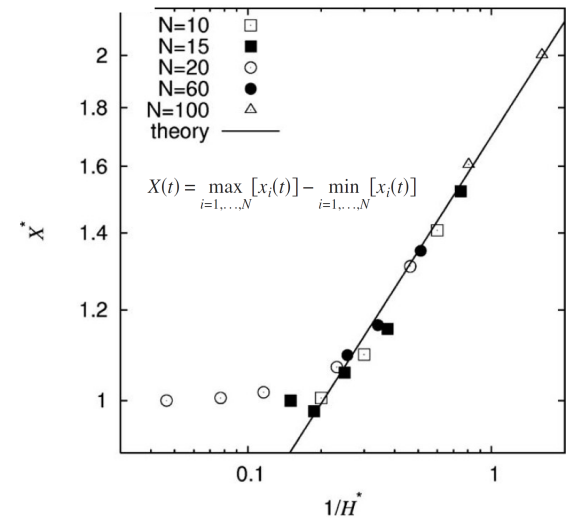
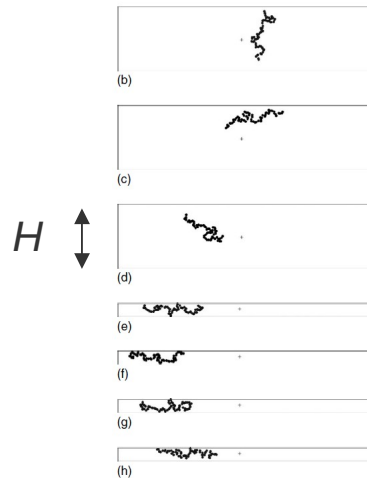
Structure factor



Internal Rouse modes



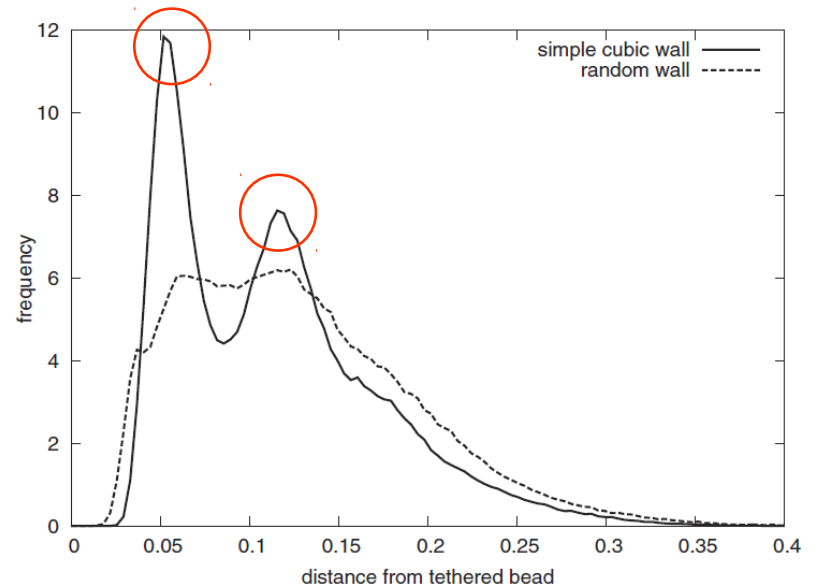
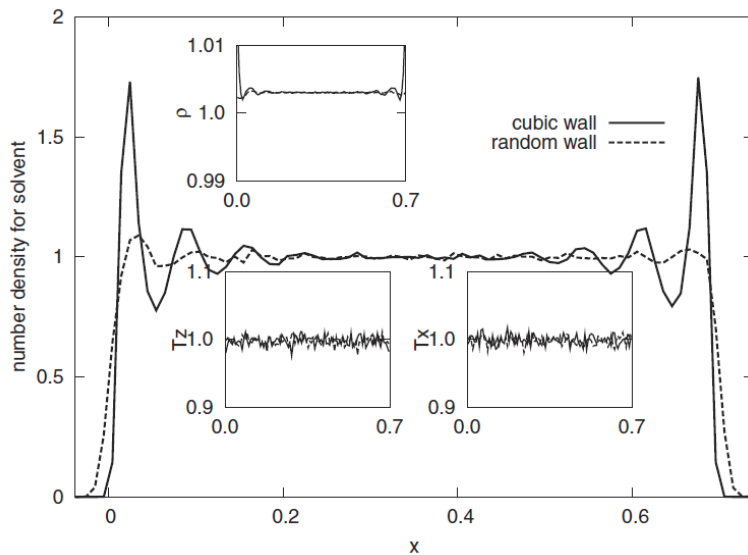
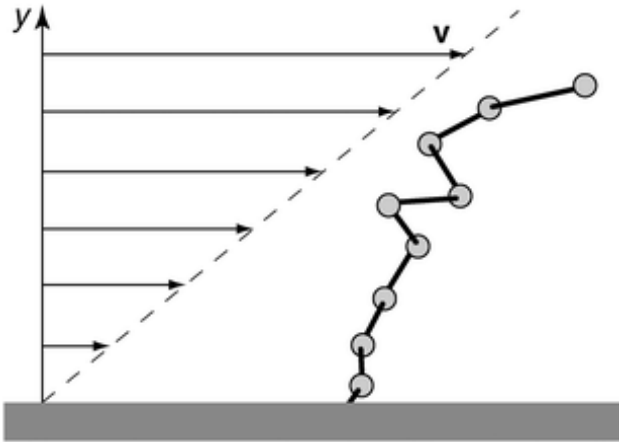
Confinement



Polymeric fluid: *mesoscopic* model

□ Tethered polymer under shear

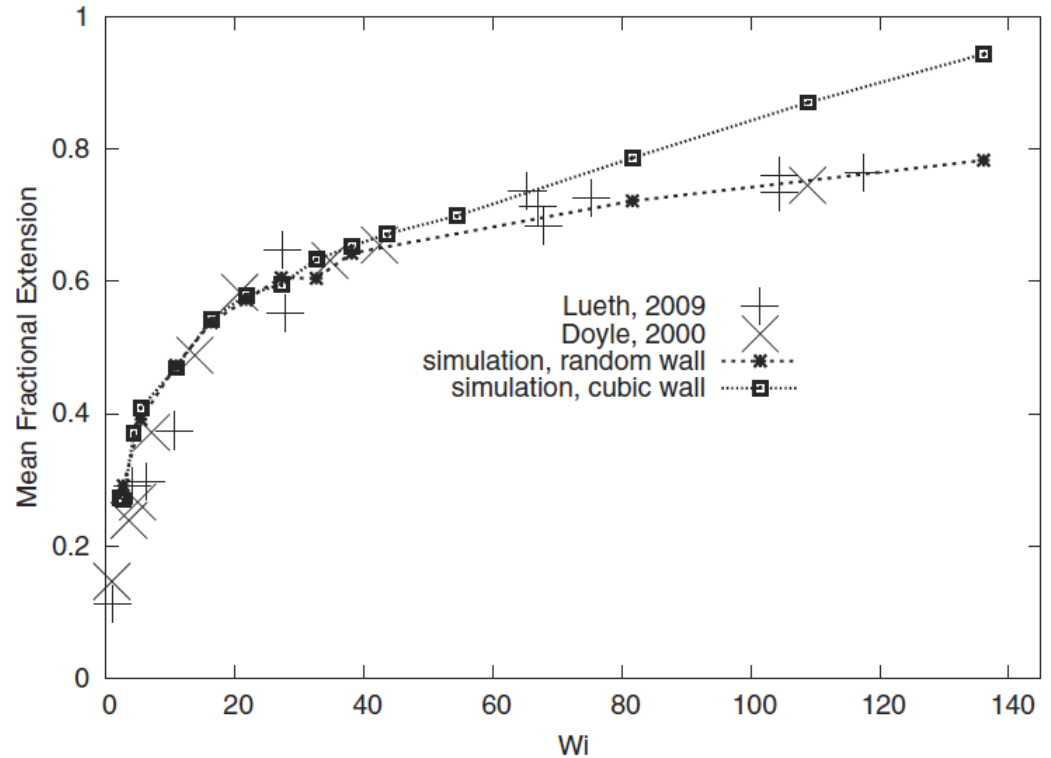
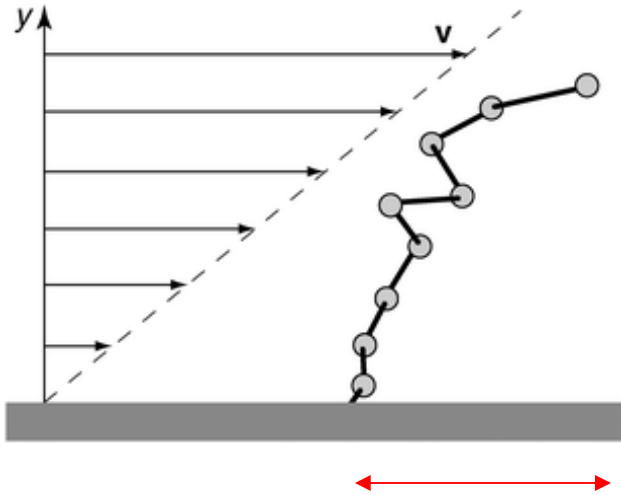
Litvinov et al., Phys.Rev. E **82**, 066704 (2010)



Polymeric fluid: *mesoscopic* model

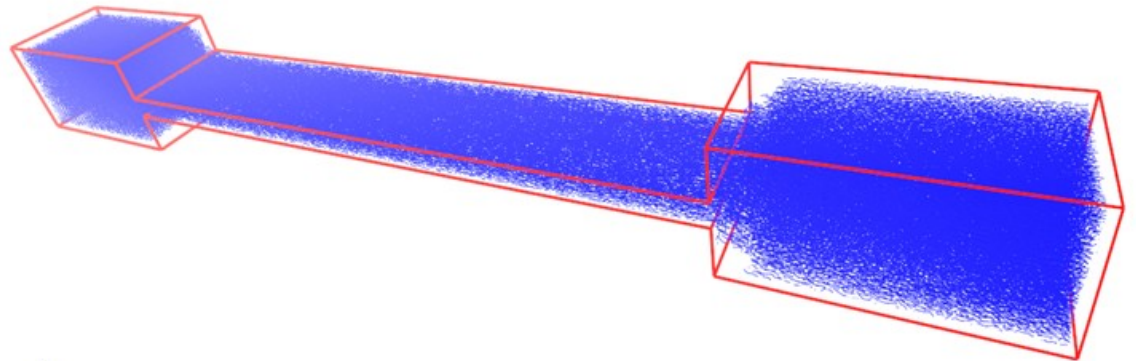
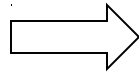
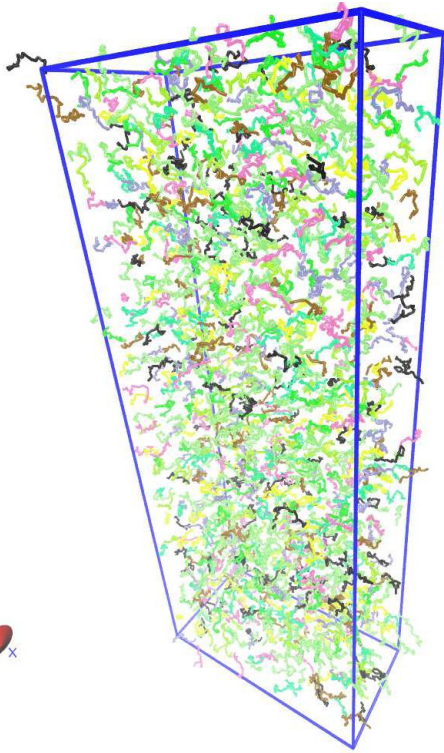
□ Tethered polymer under shear

Litvinov et al., Phys.Rev. E **82**, 066704 (2010)



Polymeric *mesoscopic* model: applications

- Rheology/collective dynamics
(DNS – no need of constitutive equation)

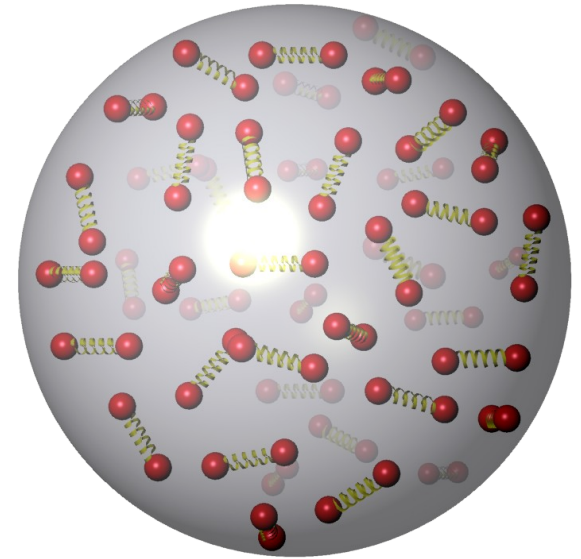
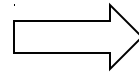
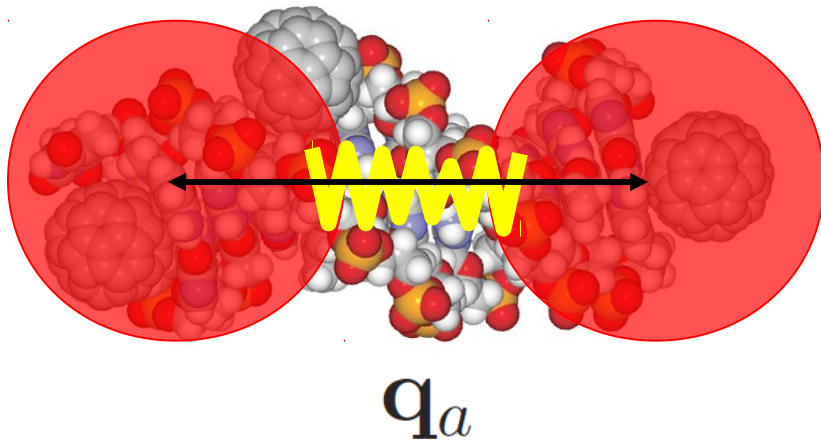


Litvinov et al., *Microfluidics Nanofluidics* **16**, 257-264 (2014)

II: Coarse-graining

Polymeric fluid: ***coarse-graining*** model

Polymeric fluid: *coarse-graining* model



Langevin equation (Brownian Dynamics)

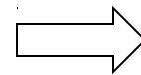
$$d\mathbf{q}_a = \underbrace{(\nabla \mathbf{v})_i^T \cdot \mathbf{q}_a dt}_{\text{flow stretching}} + \underbrace{\frac{2\mathbf{F}(\mathbf{q}_a)}{\gamma}}_{\text{elastic recoil}} dt + \underbrace{d\tilde{\mathbf{q}}_a}_{\text{thermal noise}}$$

$$d\tilde{\mathbf{q}}_a d\tilde{\mathbf{q}}_b = \delta_{ab} 4D_0 \mathbf{1} dt$$

Coarse-grained variable: **conformation tensor**

$$\mathbf{c}_i = \frac{1}{N_p q_0^2} \sum_{a=1}^{N_p} \mathbf{q}_a \mathbf{q}_a$$

$d\mathbf{c}_i = ?$



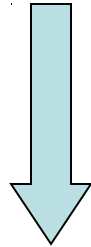
Polymeric fluid: *coarse-graining* model

Vazquez, Ellero, Espanol, Phys.Rev. E **79**, 056707 (2009)

$$d\mathbf{q}_a = \underbrace{(\nabla \mathbf{v})_i^T \cdot \mathbf{q}_a dt + \frac{2\mathbf{F}(\mathbf{q}_a)}{\gamma} dt}_{\text{Hookean spring}} + d\tilde{\mathbf{q}}_a$$

$$d\tilde{\mathbf{q}}_a d\tilde{\mathbf{q}}_b = \delta_{ab} 4D_0 \mathbf{1} dt$$

Hookean spring

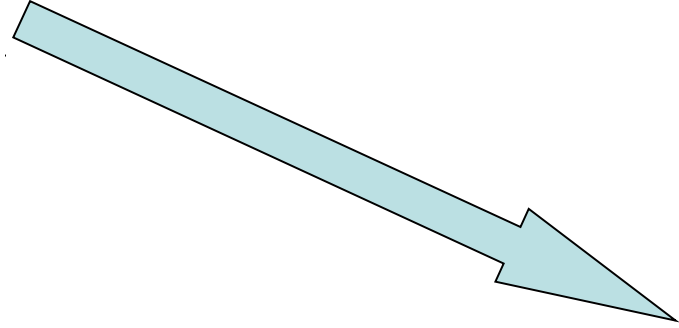


$$d\mathbf{c}_i = -\mathbf{c}_i \cdot \underbrace{\left(\sum_j \nu_j W'_{ij} \mathbf{v}_{ij} \mathbf{e}_{ij} \right)}_{\nabla \mathbf{v}_i} dt - \left(\sum_j \nu_j W'_{ij} \mathbf{v}_{ij} \mathbf{e}_{ij} \right)^T \cdot \mathbf{c}_i dt + \frac{1}{\tau} [\mathbf{1} - \mathbf{c}_i] dt$$

Polymeric fluid: *coarse-graining* model

Vazquez, Ellero, Espanol, Phys.Rev. E **79**, 056707 (2009)

$$d\mathbf{q}_a = (\nabla \mathbf{v})_i^T \cdot \mathbf{q}_a dt + \frac{2\mathbf{F}(\mathbf{q}_a)}{\gamma} dt + \underbrace{d\tilde{\mathbf{q}}_a}_{d\tilde{\mathbf{q}}_a d\tilde{\mathbf{q}}_b = \delta_{ab} 4D_0 \mathbf{1} dt}$$



$$d\mathbf{c}_i = -\mathbf{c}_i \cdot \underbrace{\left(\sum_j \nu_j W'_{ij} \mathbf{v}_{ij} \mathbf{e}_{ij} \right)}_{\nabla \mathbf{v}_i} dt - \left(\sum_j \nu_j W'_{ij} \mathbf{v}_{ij} \mathbf{e}_{ij} \right)^T \cdot \mathbf{c}_i dt + \frac{1}{\tau} [\mathbf{1} - \mathbf{c}_i] dt + \underbrace{d\tilde{\mathbf{c}}_i}_{\text{Tensorial Wiener process}}$$

Tensorial Wiener process

$$\langle d\tilde{c}^{\alpha\beta} d\tilde{c}^{\alpha'\beta'} \rangle = \frac{dt}{N_p \tau} \left[c^{\alpha\alpha'} \delta^{\beta\beta'} + c^{\alpha'\beta} \delta^{\alpha\beta'} + c^{\alpha\beta'} \delta^{\beta\alpha'} + c^{\beta'\beta} \delta^{\alpha\alpha'} \right]$$

Polymeric fluid: *coarse-graining* model

Vazquez, Ellero, Espanol, Phys.Rev. E **79**, 056707 (2009)

$$\begin{aligned}\dot{\mathbf{r}}_i &= \mathbf{v}_i \\ m\dot{\mathbf{v}}_i &= \sum_j \left(\frac{\boldsymbol{\Pi}_i}{d_i^2} + \frac{\boldsymbol{\Pi}_j}{d_j^2} \right) W'_{ij} \mathbf{e}_{ij} + \frac{5\eta}{3} \sum_j \frac{W'_{ij}}{d_i d_j r_{ij}} [\mathbf{v}_{ij} + (\mathbf{e}_{ij} \cdot \mathbf{v}_{ij}) \mathbf{e}_{ij}] + \sum_j A_{ij} \frac{d\bar{\boldsymbol{\xi}}_{ij}}{dt} \cdot \mathbf{e}_{ij} \\ d\mathbf{c}_i &= -\mathbf{c}_i \cdot \left(\sum_j \nu_j W'_{ij} \mathbf{v}_{ij} \mathbf{e}_{ij} \right) dt - \left(\sum_j \nu_j W'_{ij} \mathbf{v}_{ij} \mathbf{e}_{ij} \right)^T \cdot \mathbf{c}_i dt + \frac{1}{\tau} [\mathbf{1} - \mathbf{c}_i] dt + d\tilde{\mathbf{c}}_i\end{aligned}$$

$$\boldsymbol{\Pi}_i = -P_i \mathbf{1} + n_p k_B T \mathbf{c}_i$$

Polymeric fluid: *coarse-graining* model

Vazquez, Ellero, Espanol, Phys.Rev. E **79**, 056707 (2009)

$$\begin{aligned}\dot{\mathbf{r}}_i &= \mathbf{v}_i \\ m\dot{\mathbf{v}}_i &= \sum_j \left(\frac{\boldsymbol{\Pi}_i}{d_i^2} + \frac{\boldsymbol{\Pi}_j}{d_j^2} \right) W'_{ij} \mathbf{e}_{ij} + \frac{5\eta}{3} \sum_j \frac{W'_{ij}}{d_i d_j r_{ij}} [\mathbf{v}_{ij} + (\mathbf{e}_{ij} \cdot \mathbf{v}_{ij}) \mathbf{e}_{ij}] + \sum_j A_{ij} \frac{d\bar{\boldsymbol{\xi}}_{ij}}{dt} \cdot \mathbf{e}_{ij} \\ d\mathbf{c}_i &= -\mathbf{c}_i \cdot \left(\sum_j \nu_j W'_{ij} \mathbf{v}_{ij} \mathbf{e}_{ij} \right) dt - \left(\sum_j \nu_j W'_{ij} \mathbf{v}_{ij} \mathbf{e}_{ij} \right)^T \cdot \mathbf{c}_i dt + \frac{1}{\tau} [\mathbf{1} - \mathbf{c}_i] dt + d\tilde{\mathbf{c}}_i\end{aligned}$$

$$\boldsymbol{\Pi}_i = -P_i \mathbf{1} + n_p k_B T \mathbf{c}_i$$

$$d\mathbf{x} = \mathbf{L} \cdot \frac{\partial E}{\partial \mathbf{x}} dt$$

Thermodynamic consistent (GENERIC)

Polymeric fluid: *coarse-graining* model

Vazquez, Ellero, Espanol, Phys.Rev. E **79**, 056707 (2009)

$$\begin{aligned}\dot{\mathbf{r}}_i &= \mathbf{v}_i \\ m\dot{\mathbf{v}}_i &= \sum_j \left(\frac{\boldsymbol{\Pi}_i}{d_i^2} + \frac{\boldsymbol{\Pi}_j}{d_j^2} \right) W'_{ij} \mathbf{e}_{ij} + \frac{5\eta}{3} \sum_j \frac{W'_{ij}}{d_i d_j r_{ij}} [\mathbf{v}_{ij} + (\mathbf{e}_{ij} \cdot \mathbf{v}_{ij}) \mathbf{e}_{ij}] + \sum_j A_{ij} \frac{d\bar{\boldsymbol{\xi}}_{ij}}{dt} \cdot \mathbf{e}_{ij} \\ d\mathbf{c}_i &= -\mathbf{c}_i \cdot \left(\sum_j \nu_j W'_{ij} \mathbf{v}_{ij} \mathbf{e}_{ij} \right) dt - \left(\sum_j \nu_j W'_{ij} \mathbf{v}_{ij} \mathbf{e}_{ij} \right)^T \cdot \mathbf{c}_i dt + \frac{1}{\tau} [\mathbf{1} - \mathbf{c}_i] dt + d\tilde{\mathbf{c}}_i\end{aligned}$$

$$\boldsymbol{\Pi}_i = -P_i \mathbf{1} + n_p k_B T \mathbf{c}_i$$

$$d\mathbf{x} = \mathbf{L} \cdot \frac{\partial E}{\partial \mathbf{x}} dt + \mathbf{M} \cdot \frac{\partial S}{\partial \mathbf{x}} dt$$

Thermodynamic consistent (GENERIC)

Polymeric fluid: *coarse-graining* model

Vazquez, Ellero, Espanol, Phys.Rev. E **79**, 056707 (2009)

$$\begin{aligned} \dot{\mathbf{r}}_i &= \mathbf{v}_i \\ m\dot{\mathbf{v}}_i &= \sum_j \left(\frac{\boldsymbol{\Pi}_i}{d_i^2} + \frac{\boldsymbol{\Pi}_j}{d_j^2} \right) W'_{ij} \mathbf{e}_{ij} + \frac{5\eta}{3} \sum_j \frac{W'_{ij}}{d_i d_j r_{ij}} [\mathbf{v}_{ij} + (\mathbf{e}_{ij} \cdot \mathbf{v}_{ij}) \mathbf{e}_{ij}] + \sum_j A_{ij} \frac{d\bar{\boldsymbol{\xi}}_{ij}}{dt} \cdot \mathbf{e}_{ij} \\ d\mathbf{c}_i &= -\mathbf{c}_i \cdot \left(\sum_j \nu_j W'_{ij} \mathbf{v}_{ij} \mathbf{e}_{ij} \right) dt - \left(\sum_j \nu_j W'_{ij} \mathbf{v}_{ij} \mathbf{e}_{ij} \right)^T \cdot \mathbf{c}_i dt + \frac{1}{\tau} [\mathbf{1} - \mathbf{c}_i] dt + d\tilde{\mathbf{c}}_i \end{aligned}$$

$$\boldsymbol{\Pi}_i = -P_i \mathbf{1} + n_p k_B T \mathbf{c}_i$$

$$d\mathbf{x} = \mathbf{L} \cdot \frac{\partial E}{\partial \mathbf{x}} dt + \mathbf{M} \cdot \frac{\partial S}{\partial \mathbf{x}} dt + d\tilde{\mathbf{x}}$$

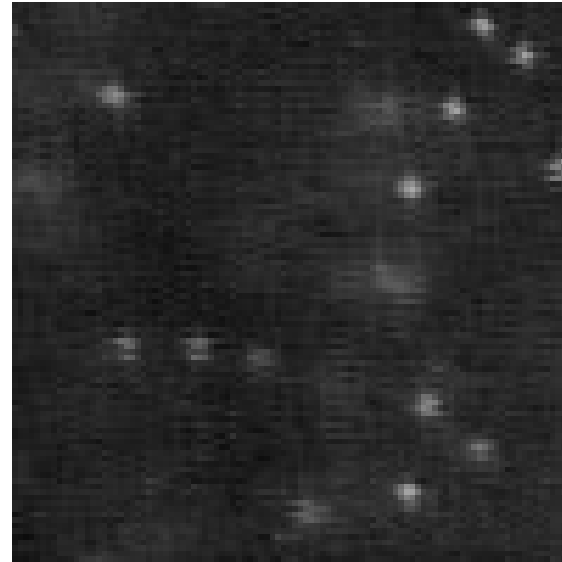
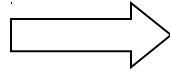
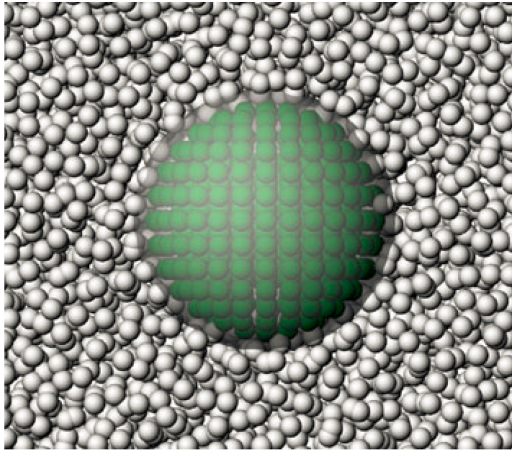


Thermodynamic consistent (GENERIC)

$$d\tilde{\mathbf{x}} d\tilde{\mathbf{x}}^T = 2k_B \mathbf{M} dt$$

Polymeric fluid: *coarse-graining* model

- ❑ SDPD: Coarse-grained viscoelasticity + Brownian motion
- ❑ Application: Passive microrheology
(correct diffusional dynamics for a nanoparticle in a polymeric liquid)

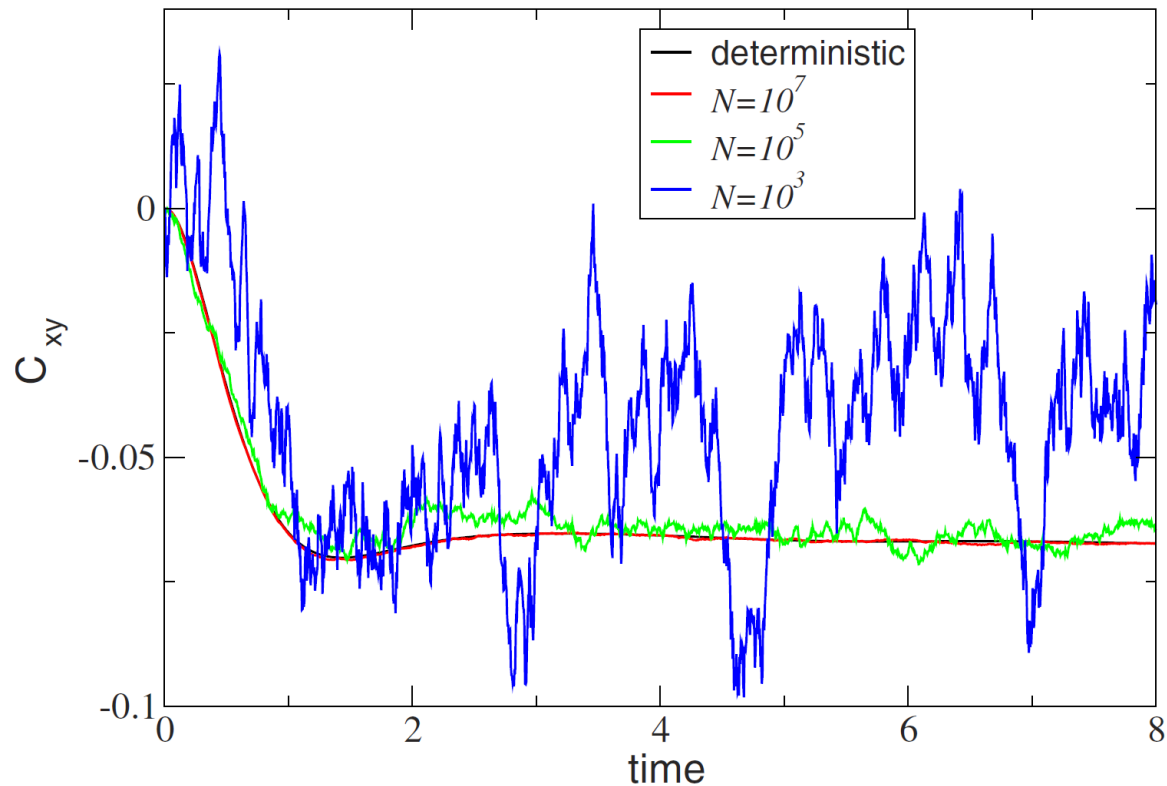


III: Towards continuum

Polymeric fluid: *coarse-graining* model

Vazquez, Ellero, Espanol, Phys.Rev. E **79**, 056707 (2009)

$$\langle d\tilde{c}^{\alpha\beta} d\tilde{c}^{\alpha'\beta'} \rangle = \frac{dt}{N_p\tau} \left[c^{\alpha\alpha'} \delta^{\beta\beta'} + c^{\alpha'\beta} \delta^{\alpha\beta'} + c^{\alpha\beta'} \delta^{\beta\alpha'} + c^{\beta'\beta} \delta^{\alpha\alpha'} \right]$$



Polymeric fluid: *macroscopic continuum* model

$$d\mathbf{c}_i = -\mathbf{c}_i \cdot \left(\sum_j \nu_j W'_{ij} \mathbf{v}_{ij} \mathbf{e}_{ij} \right) dt - \left(\sum_j \nu_j W'_{ij} \mathbf{v}_{ij} \mathbf{e}_{ij} \right)^T \cdot \mathbf{c}_i dt + \frac{1}{\tau} [\mathbf{1} - \mathbf{c}_i] dt + d\tilde{\mathbf{c}}_i$$

$$\nu_i = \left(\sum_j W_{ij} \right) \longrightarrow \infty \qquad \longrightarrow 0$$

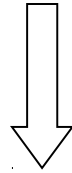
Fluid particle volume

$$\lim_{\nu_i \rightarrow \infty} \text{SDPD} = \text{SPH}$$

Polymeric fluid: *macroscopic continuum* model

$$d\mathbf{c}_i = -\mathbf{c}_i \cdot \left(\sum_j \nu_j W'_{ij} \mathbf{v}_{ij} \mathbf{e}_{ij} \right) dt - \left(\sum_j \nu_j W'_{ij} \mathbf{v}_{ij} \mathbf{e}_{ij} \right)^T \cdot \mathbf{c}_i dt + \frac{1}{\tau} [\mathbf{1} - \mathbf{c}_i] dt$$

SPH discretization



□ **Oldroyd-B viscoelastic PDE** (conformation tensor representation: Huelsen et al. 1987)

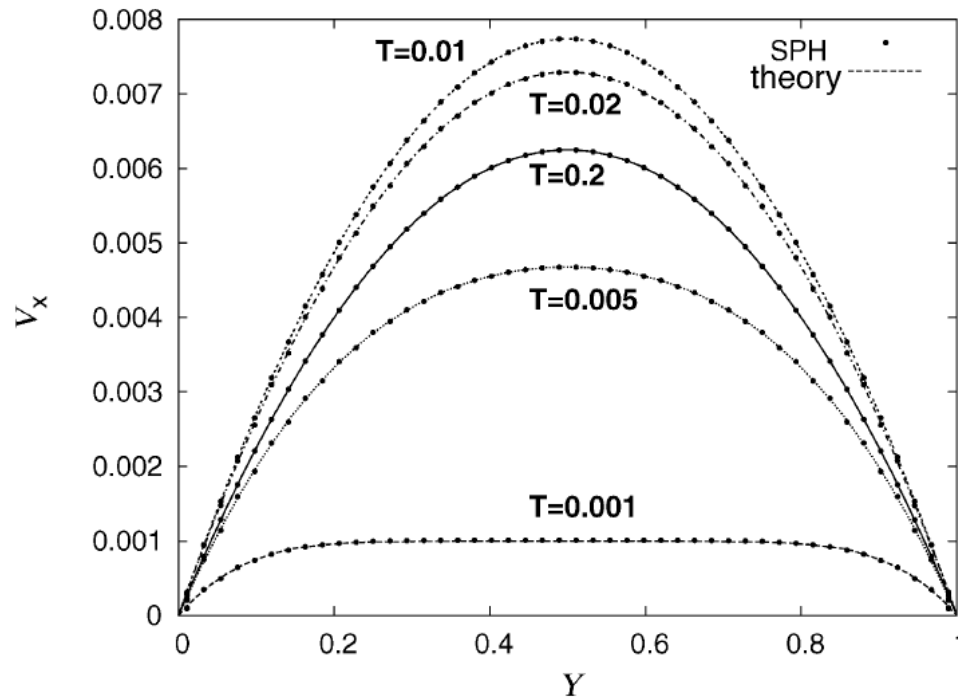
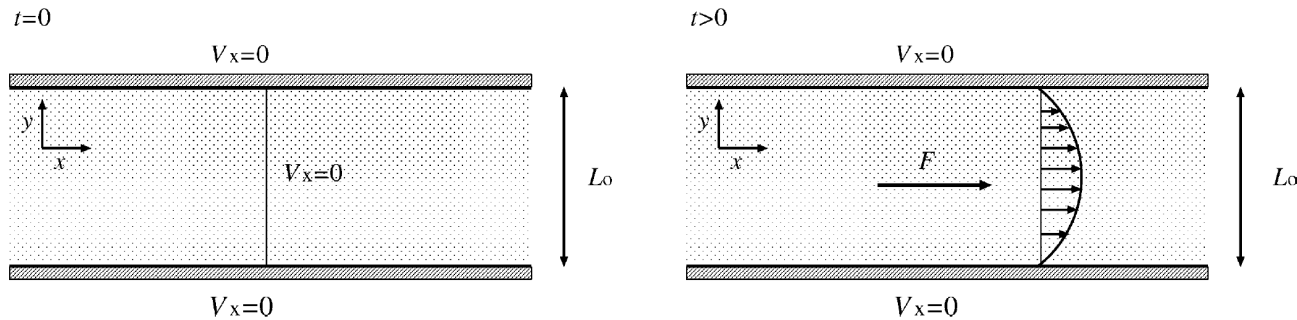
$$\frac{\partial \mathbf{c}}{\partial t} + \mathbf{v} \cdot \nabla \mathbf{c} = \underbrace{(\nabla \mathbf{v})^T \cdot \mathbf{c} + \mathbf{c} \cdot (\nabla \mathbf{v})}_{\text{flow stretching}} + \underbrace{\frac{1}{\lambda} [\mathbf{1} - \mathbf{c}]}_{\text{polymer relaxation}}$$

Oldroyd, James "On the Formulation of Rheological Equations of State".
Proceedings of the Royal Society of London, A, **200** (1063): 523–541 (1950)

Polymeric fluid: *macroscopic continuum* model

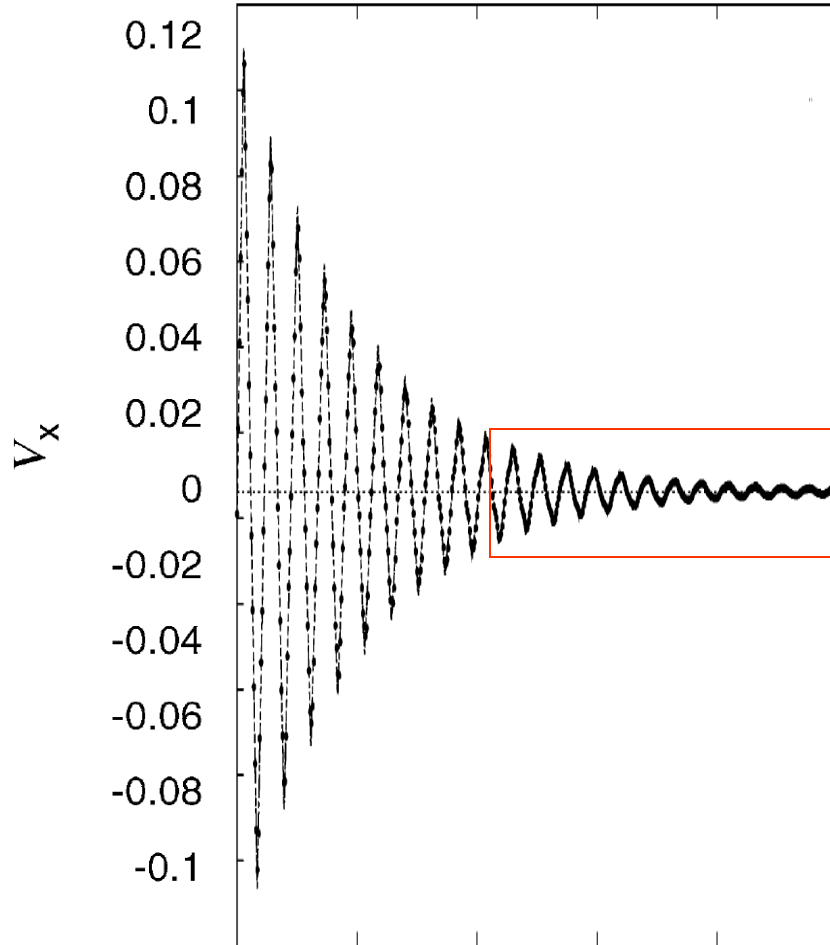
□ Oldroyd-B transient simulations [start-up Poiseuille flow]

Ellero, Tanner, J. Non-NewtFluid. Mech. **132**, 61 (2005)
Smoothed Particle Hydrodynamics

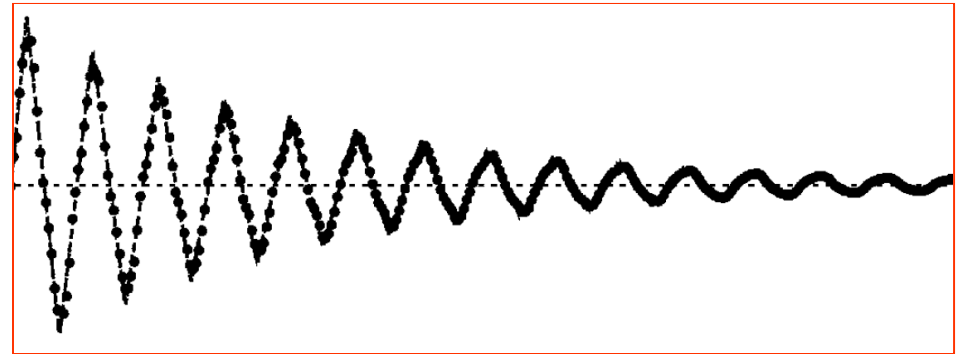


Polymeric fluid: *macroscopic continuum* model

- **Oldroyd-B transient simulations**
[start-up Poiseuille flow]



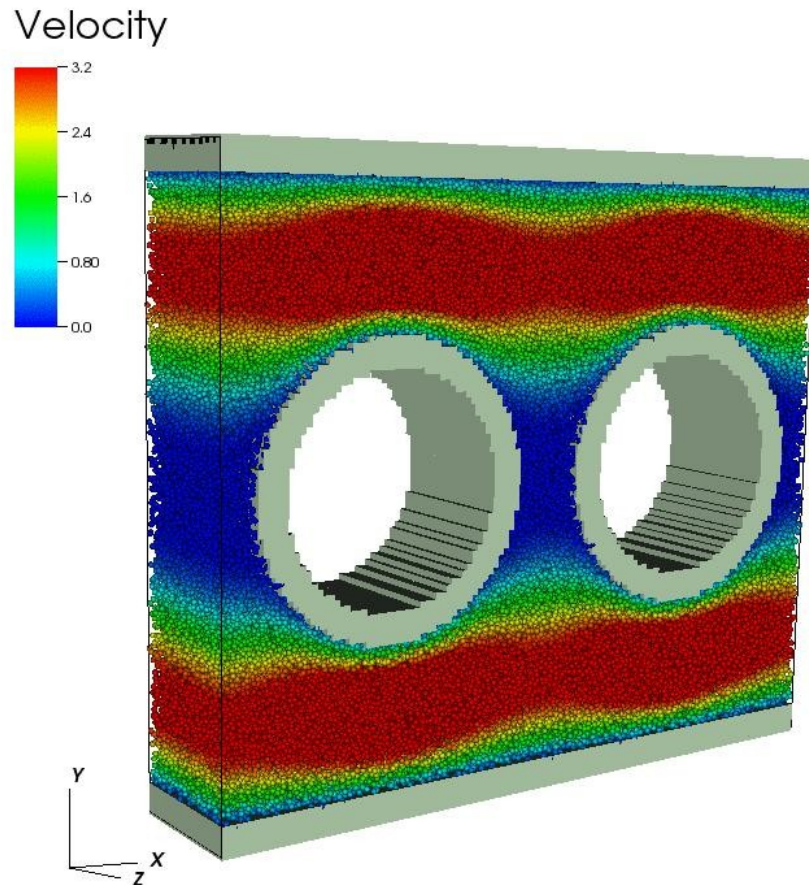
Ellero, Tanner, J. Non-NewtFluid. Mech. **132**, 61 (2005)
Smoothed Particle Hydrodynamics



Polymeric fluid: *macroscopic continuum* model

□ Flow in around micro-array of cylinders

Grilli, Vazquez, Ellero, Phys. Rev. Lett. **110**, 174501 (2013)

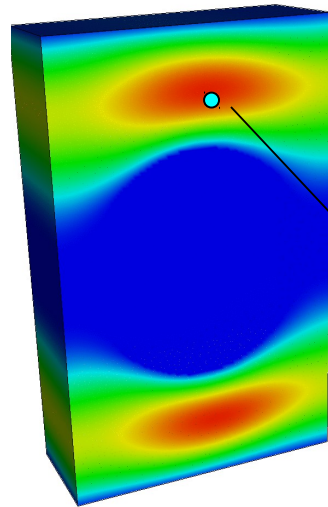
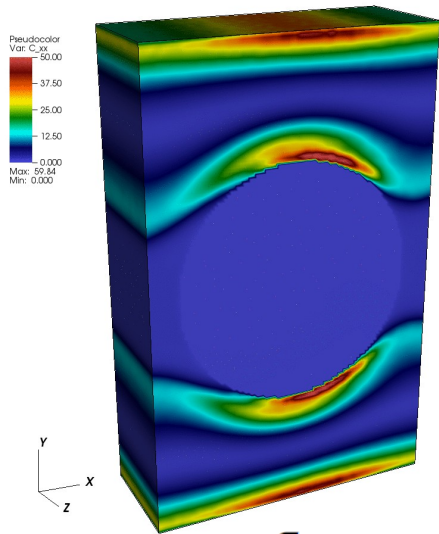
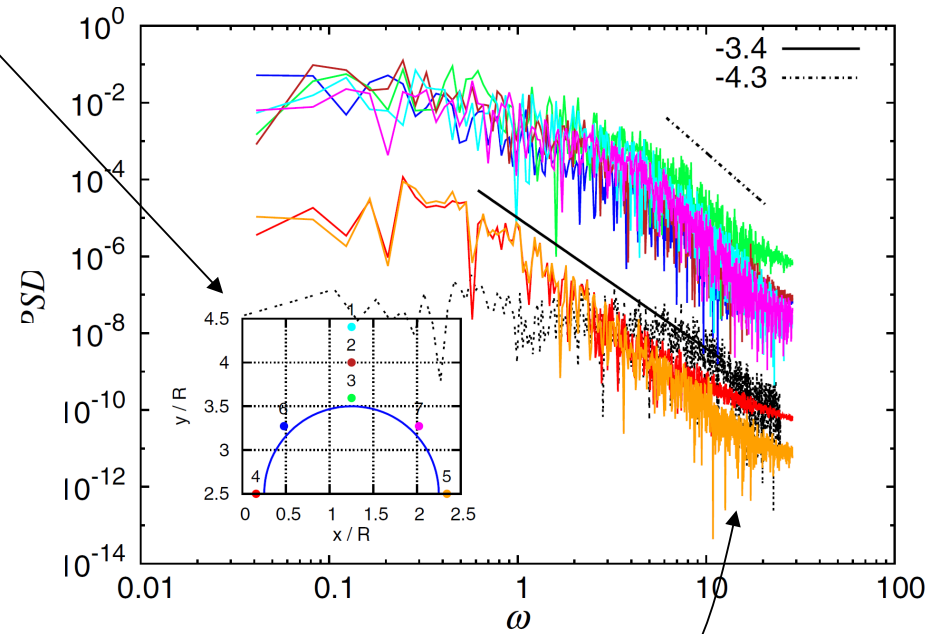


Polymeric fluid: *macroscopic continuum* model

Grilli, Vazquez, Ellero, Phys. Rev. Lett. **110**, 174501 (2013)

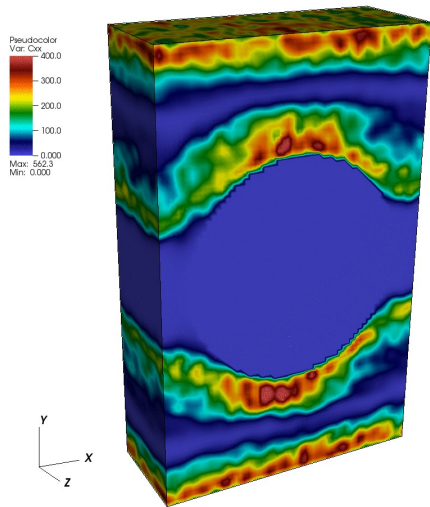
We=0.42

Power spectral density

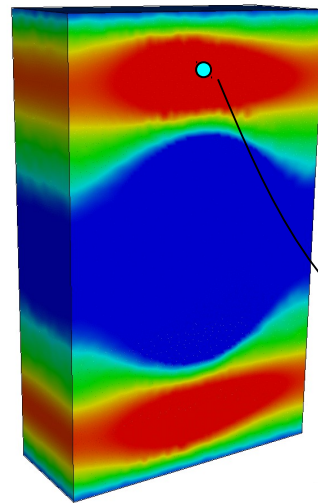


τ_{xx}

v_x



Pseudocolor
Var: Vel_y
Max: 2.951
Min: -0.05886



We=1.3

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Elastic turbulence

NATURE | VOL 405 | 4 MAY 2000

Elastic turbulence in a polymer solution flow

A. Groisman & V. Steinberg

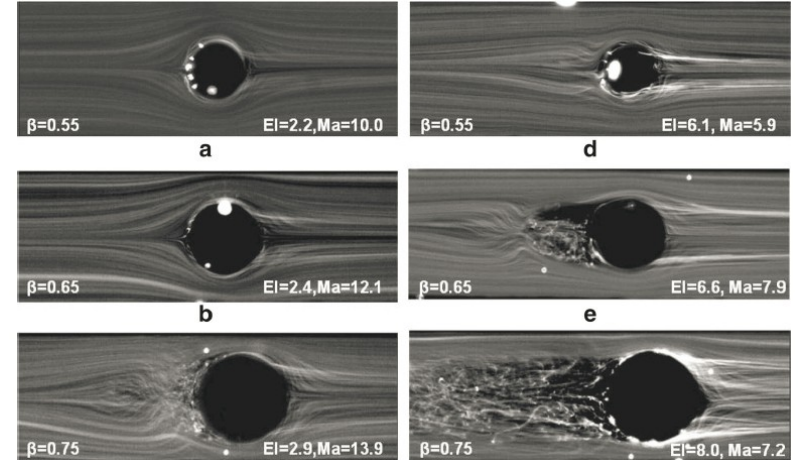
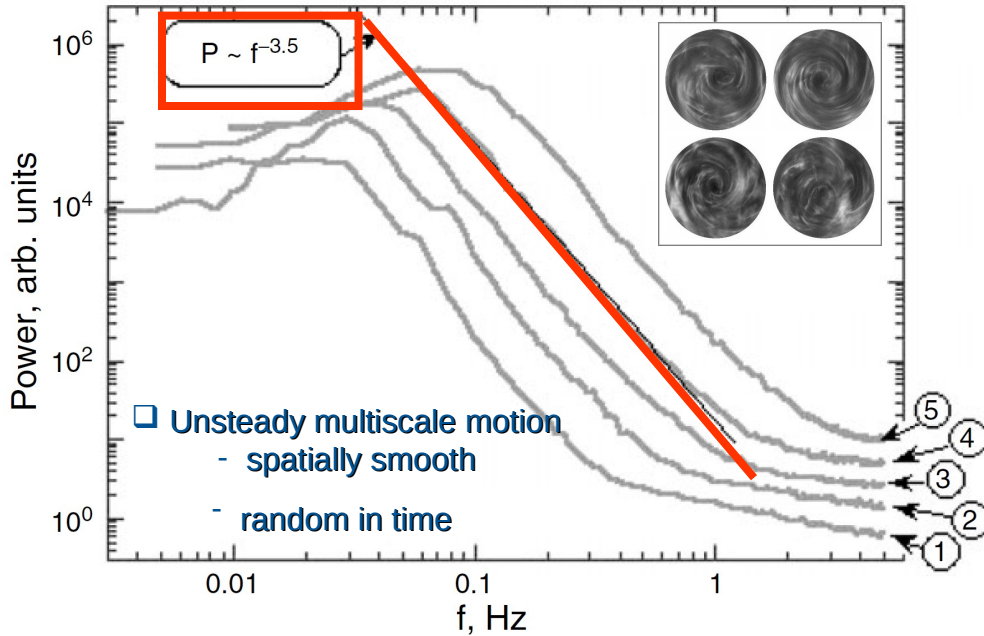
Rheol Acta
DOI 10.1007/s00397-015-0875-6

ORIGINAL CONTRIBUTION

Mechanisms of onset for moderate Mach number instabilities of viscoelastic flows around confined cylinders

Xueda Shi¹ · Stephen Kenney¹ · Ganesh Chapagain¹ · Gordon F. Christopher¹

Received: 6 March 2015 / Revised: 20 August 2015 / Accepted: 24 August 2015
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- Power-law decay
- Talyor's hypothesis: $E(k) \sim k^{-\alpha}$ $\alpha > 3$

Lebedev PRE 2003 (theory $\rightarrow >3!!$)

Conclusions

- ❑ **SDPD for simple Newtonian solvents: improved DPD version.**
 - control transport coefficients
 - arbitrary thermodynamic behaviour EOS, incompressibility
 - thermodynamic def. particle volume: resolution analysis straightforward
- ❑ **Consistent scaling of thermal fluctuations: SDPD → SPH : “large” particle volumes**
- ❑ **Complex fluids: SDPD versatile approach → hierarchical modelling**
- ❑ **Mesosopic models possible as DPD (albeit with better defined solvent properties).**
- ❑ **Coarse-graining approach offer scale advantage (under some approx).**
- ❑ **Consistent scaling: SDPD → SPH specific discretization continuum viscoelastic PDE**
 - e.g. Hookean spring dumbbells → Oldroyd-B
- ❑ **Embedded in GENERIC: (i) 1st Law; (ii) 2nd Law; (ii) FDT exactly satisfied.**